In the Claims:

Claims 1-41 (Cancelled)

42. (Previously Presented): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H_2O with a low-pyrophoricity water-gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m^2/g impregnated with:

(i) 0.5 to 25% by weight of an oxide of Ce, calculated as CeO_2, impregnated in the support particles, and

(ii) between 4 and 14% by weight catalytic agent wherein the catalytic agent is Cu or an oxide thereof, calculated as CuO.

43. (Previously Presented): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H_2O with a low-pyrophoricity water-gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m^2/g impregnated with:

(i) 0.5 to 25% by weight of an oxide of cerium, calculated as CeO_2 impregnated in the support particles;

(ii) 0.5 to 10% by weight of an oxide of chromium, calculated as Cr_2O_3, impregnated in the support particles; wherein the combined concentration of the oxides of cerium and chromium is between 0.5 to 35% by weight; and

(iii) between 4 and 14% by weight catalytic agent, wherein the catalytic agent is copper or an oxide thereof, calculated as CuO.

44. (Cancelled)

45. (Previously Presented): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H_2O with a low-pyrophoricity water-

gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m^2/g impregnated with:

(i) 0.5 to 15% by weight of an oxide of chromium, calculated as Cr_2O_3, impregnated in the support particles, and

(ii) between 4 and 14% by weight catalytic agent wherein the catalytic agent is Cu or an oxide thereof, calculated as CuO.

46. (Previously Presented): The process of claim 42, wherein the input gas stream comprises:

(i) between about 1% by volume and about 10% by volume CO,

(ii) at least 10% by volume hydrogen, and

(iii) at least 10% by volume H_2O; and

wherein the input gas stream has a space velocity of at least 500 hr^{-1} VHSV.

47. (Previously Presented): The process of claim 43, wherein the input gas stream comprises:

(i) between about 1% by volume and about 10% by volume CO,

(ii) at least 10% by volume hydrogen, and

(iii) at least 10% by volume H_2O; and

wherein the input gas stream has a space velocity of at least 500 hr^{-1} VHSV.

48. (Previously Presented): The process of claim 45, wherein the input gas stream comprises:

(i) between about 1% by volume and about 10% by volume CO,

(ii) at least 10% by volume hydrogen, and

(iii) at least 10% by volume H_2O; and

wherein the input gas stream has a space velocity of at least 500 hr^{-1} VHSV.